

**Amendments to the Claims:**

This listing of claims will replace all prior versions, and listings, of claims in the application:

**Listing of Claims:**

Claims 1-10 (Canceled)

Claim 11 (Currently Amended): A process for purifying on a large scale a product from a feedstock containing one or more impurities having closely-related physical properties to the product, which process comprises:

feeding the feedstock into an extraction column under conditions adapted for separating more-or-less polar impurities from the feedstock, wherein a lighter phase flows counter to a heavier phase, thereby forming an output in one phase containing the product containing less more- or less-polar impurities so that the output contains the product in a substantially purified form, wherein the lighter phase comprises heptane and acetone or heptane and isopropanol, the heavier phase comprises water and acetone or water and isopropanol, and the product is [[a]] rapamycin or a derivative thereof or [[an]] ascomycin or a derivative thereof.

Claim 12 (Previously Presented): A process of claim 11, wherein the lighter phase comprises about 25 wt-% n-heptane and about 75 wt-% acetone, or about 90 wt-% n-heptane and about 10 wt-% isopropanol.

Claim 13 (Previously Presented): A process of Claim 11, wherein the heavier phase comprises about 50 wt-% water and about 50 wt-% acetone, or about 68 wt-% water and about 32 wt-% isopropanol.

Claim 14 (Withdrawn): A process for purifying on a large scale a product from a feedstock containing one or more impurities having closely-related physical properties to the product, which process comprises the steps of

- a) feeding the feedstock into a first extraction column under conditions adapted for separating more- or less-polar impurities from the feedstock, wherein a lighter phase flows counter to a heavier phase, thereby forming a first output in one phase containing the product containing less more- or less-polar impurities, and
- b) feeding the first-output into a second extraction column under conditions adapted for separating less- or more-polar impurities respectively from the first output, wherein the lighter phase flows counter to the heavier phase, thereby forming in one phase a second output, so that the second output contains the product in a substantially purified form, wherein the lighter phase comprises heptane and acetone or heptane and isopropanol, the heavier phase comprises water and acetone or water and isopropanol, and the product is ~~a cyclosporin~~ rapamycin or a derivative thereof or ascomycin or a derivative thereof.

Claim 15 (Withdrawn): A process of Claim 14, wherein the lighter phase comprises about 25 wt-% n-heptane and about 75 wt-% acetone, or about 90 wt-% n-heptane and about 10 wt-% isopropanol.

Claim 16 (Withdrawn): A process of claim 14, wherein the heavier phase comprises about 50 wt-% water and about 50 wt-% acetone, or about 68 wt-% water and about 32 wt-% isopropanol.

Claim 17 (Currently Amended): A process of claim 11, wherein the product is rapamycin, 40-O-(2-hydroxy)ethyl rapamycin, ascomycin, 33-epi-chloro-33-desoxyascomycin, 5,6-dehydro-ascomycin or FK506.

Claim 18 (Withdrawn): A countercurrent extraction column having between 100 and 200 compartments, and an overall efficiency of about 10 to 30%.

Claim 19 (Cancelled)

Claim 20 (Cancelled)

Claim 21 (Cancelled)

Claim 22 (Cancelled)